

**Partial test**  
**SCE1106 Control Theory**  
**Tuesday 21. October 2008**  
**kl. 10.15-12.15, Rom F29**

The test consists of 4 tasks.

The test counts 15% =  $0.5 * 30$  % of the final grade  
in SCE1106 Control with implementation.

The test consists of three pages.

Aid: paper and pen.

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## Task 1 (2%): System modeling

Given a system described by the continuous state space model

$$\dot{x} = Ax + Bu \quad (1)$$

$$y = Dx + Eu \quad (2)$$

where

$$A = -0.1, \quad B = 0.06, \quad D = 1, \quad E = -0.1 \quad (3)$$

Show that the system can be described by the transfer function model

$$y = h_p(s)u \quad (4)$$

where

$$h_p(s) = k \frac{1 - \tau s}{1 + Ts} \quad (5)$$

Find the gain,  $k$ , the time constant,  $T$ , and the inverse response time constant,  $\tau$ , in the transfer function model (5).

## Task 2 (12%): PID-control, the Skogestad method

We are going to study a process described by the transfer function model

$$y = h_p(s)u. \quad (6)$$

The process are to be controlled by a controller of the form

$$u = h_c(s)(r - y). \quad (7)$$

The feedback control system is illustrated in Figure (1).

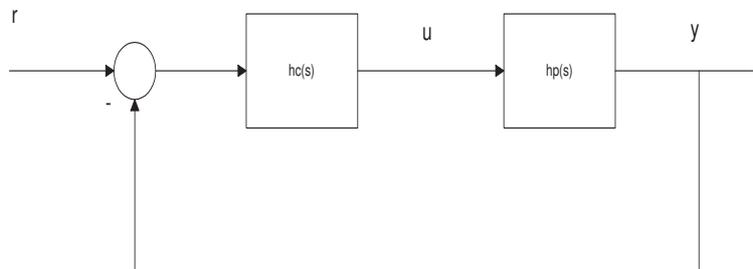


Figure 1: Standard feedback control system.

a) Consider the feedback control system in Figure (1).

- Find the transfer function from the reference,  $r$ , to the output measurement,  $y$ , i.e., find the transfer function

$$\frac{y}{r} = h_r(s) \quad (8)$$

where  $h_r(s)$  is the transfer function from  $r$  to  $y$ .

- Find an expression for the transfer function,  $h_c(s)$ , for the controller as a function of the ratio  $\frac{y}{r}$  and the transfer function for the process,  $h_p(s)$ .

We will in the following subtasks specify that the set point response from the reference,  $r$ , to the output,  $y$ , should be given by

$$\frac{y}{r} = \frac{1 - \tau s}{1 + T_c s} \quad (9)$$

where  $T_c$  is a user specified time constant.

- b) Suggest a value for the specified time constant  $T_c$  for the set point response.
- c) Assume that the process,  $h_p(s)$ , is modelled by a 2nd order transfer function given by

$$h_p(s) = k \frac{1 - \tau s}{(1 + T_1 s)(1 + T_2 s)}, \quad (10)$$

where  $T_1 > T_2 > 0$ .

Find the controller  $h_c(s)$  by the Skogestad method. What type of controller is this?

- d) Assume that the process,  $h_p(s)$ , is modelled by a 1st order model given by

$$h_p(s) = k \frac{1 - \tau s}{1 + T_1 s}. \quad (11)$$

Find the controller  $h_c(s)$  by the Skogestad method. What type of controller is this?

- e) Assume that the process,  $h_p(s)$ , is modelled by a 2nd order oscillating process of the form

$$h_p(s) = k \frac{1 - \tau s}{\tau_0^2 s^2 + 2\tau_0 \xi s + 1}. \quad (12)$$

Find the controller  $h_c(s)$  by the Skogestad method. What type of controller is this?

- f) Assume that the process is modelled by a pure time delay, i.e. with a process model

$$h_p(s) = k e^{-\tau s}. \quad (13)$$

Find the controller  $h_c(s)$  by the Skogestad method. What type of controller is this?

- g) Assume that the process is modelled by an integrator with time delay, i.e. with a process model

$$h_p(s) = k \frac{e^{-\tau s}}{s}. \quad (14)$$

Find the controller  $h_c(s)$  by the Skogestad method. What type of controller is this?

### Task 3 (8%):

#### Model reduction and the half rule

- a) Given a 5th order process  $y = h_p(s)u$  where the process transfer function,  $h_p(s)$ , is given by

$$h_p(s) = k \frac{1 - \tau s}{(1 + T_1 s)(1 + T_2 s)(1 + T_3 s)} \quad (15)$$

where  $T_1 \geq T_2 \geq T_3 > 0$ .

- Use the half rule for model reduction and find a 1st order model approximation of the form

$$h_p(s) = k \frac{1 - \tau s}{1 + T_1 s} \quad (16)$$

- Use the half rule for model reduction and find a 2nd order model approximation of the form

$$h_p(s) = k \frac{1 - \tau s}{(1 + T_1 s)(1 + T_2 s)} \quad (17)$$

- b) Given the process

$$h_p(s) = k \frac{e^{-\tau s}}{(1 + T_0 s)^3} \quad (18)$$

- Use the half rule for model reduction and find a 1st order model approximation of the form

$$h_p(s) = k \frac{1 - \tau s}{1 + T_1 s} \quad (19)$$

- Use the half rule for model reduction and find a 2nd order model approximation of the form

$$h_p(s) = k \frac{1 - \tau s}{(1 + T_1 s)(1 + T_2 s)} \quad (20)$$

## Task 4 (8%): PI control

Consider a PI controller

$$u = h_c(s)e, \quad (21)$$

where  $e$  is the controller input,  $u$  is the controller output and  $h_c(s)$  is the transfer function for the PI controller.

- a) Write down the transfer function,  $h_c(s)$ , of a PI controller.
- b) Find a continuous state space equivalent for the PI controller.
- c) Use the explicit Euler method and find a discrete time state space equivalent of the PI controller.
- d) What is the meaning of "Anti Wind Up" in connection with the implementation of a PI controller?